

RECIRCULATING FLUIDIZED BED OPERATIONS

by

MUNISH KUMAR CHANDEL

Department of Civil Engineering

Submitted in fulfillment of the requirements for the degree of

DOCTOR OF PHILOSOPHY

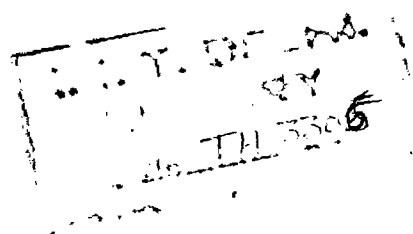
to the



INDIAN INSTITUTE OF TECHNOLOGY, DELHI

November, 2005

1. Fingerprint bed
2. RCFB

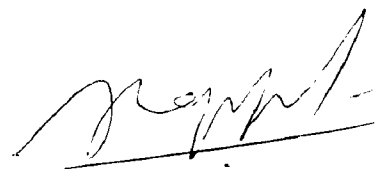


TH
624:66-912
CHA-R

CERTIFICATE

This is to certify that the thesis entitled **“Recirculating Fluidized Bed Operations”** being submitted by **Munish Kumar Chandel** to the Indian Institute of Technology, Delhi, for the award of the Degree of Doctor of Philosophy is a bonafide record of research work carried out by him under my supervision and guidance. The thesis work, in my opinion, has reached the requisite standards fulfilling the requirement for the Degree of Doctor of Philosophy.

The results contained in this thesis have not been submitted, in part or full, to any other University or Institute for the award of any degree or diploma.



(Babu J. Alappat)

Assistant Professor

Department of Civil Engineering

Indian Institute of Technology Delhi

Hauz Khas, New Delhi - 110 016

INDIA

ACKNOWLEDGEMENTS

I am delighted to express my sincere gratitude to my supervisor Dr. B. J. Alappat for his able guidance and supervision throughout my work. His knowledge of the subject and constant encouragement has helped me a lot to understand the subject. His attitude towards life, patience and modesty has changed my thinking and many aspects of life in addition to research.

I would like to thank Prof. Mukesh Khare, Prof. Manju Mohan (Center of Atmospheric Sciences), Prof. Rema Devi and Prof. S. N. Sinha for their valuable advice. My thanks are due to Dr. A. K. Mittal for his support as a Lab-in-charge. I would like to thank Dr. A. K. Nema for his suggestions and moral support.

I am thankful to Prof. K. G. Sharma, Head, Civil Engineering Department, Prof. A. K. Nagpal, Chairman, DRC, for their constant support.

I am thankful to Prof. Arnaud Delebarre and Dr. Pascaline Pre, Ecole des Mines Nantes, France for their valuable suggestions and guidance during my three months internship in France.

I would like to thank Environmental Engineering Lab staff especially Mr. Rajee Singh, Mr. Ishwar Singh, Mr. Sanjay Singh and Mr. Rajeev Sharma for their time to time help and support.

I am thankful to the workshop staff, Mr. K. K. Bali and Mr. Ram Kumar and staff of Instrument Design and Development Centre for their help in the fabrication of the reactor.

I am also thankful to the office staff, Mr. Bikram Singh, Mr. Rajveer Aggarwal and others, Civil Engineering Department for their kind help.

I would like to thank Prof. Arun Kanda, In-charge, Educational Technology Services Centre for permitting the videography required for the study of the reactor. I have great pleasure in expressing my sincere thanks to Mr Taneja, Mr. Sarwan and other staff members of the Educational Technology Services Centre for their kind help on the videographic study.

I am thankful to Dr. Inderdeep Singh for giving me good ideas for the research work. I would like to express my gratitude to Dr. Amit Kumar Agarwal and Varun Dogar for his help and motivation during my early years of PhD.

I am glad to acknowledge the help, support and motivation of my friends Anju, Vikash, Anand, Asheesh, Bharat, Vikram and Manmohan. Without them, it's difficult to imagine the completion of this work

I am also grateful to all my fellow research scholars; especially Sandeep Chaudhary, Umesh Pendhalkar, Dinesh Kumar and Sharad Gokhale for their kind help and support in my course of stay in IIT.

I would like to extend my indebtedness to all people who helped me in one way or other and made my research work a contented passage.

I wish to express my deep sense of gratitude to my parents, brother, sister and other family members for their sacrifices, encouragement and help.

I am grateful to all my teachers due to them I am here to write this thesis. Finally, I am thankful to The Almighty who created us.

A handwritten signature in black ink, appearing to read 'MK Chandel', enclosed within a circular stamp.

(Munish Kumar Chandel)

November, 2005

ABSTRACT

Fluidized bed reactors are used extensively these days for a multitude of processes including environmental pollution control and minimization. Recirculating fluidized bed (RCFB) is a type of circulating fluidized bed. RCFBs are in use for a variety of operations and processes due to the possibility of accurate control of solid circulation and the flexibility in its design and operation. The concept of RCFB is widely applied in different processes such as coating tablets, granulations and agglomeration of fine powders, grain drying, blending and mixing, low temperature carbonization of coal, devolatilization of coking coal and heavy crude oil gasification. In the field of environmental engineering, RCFB can be used for gasification and incineration of hazardous and non-hazardous wastes and flue gas desulphurization.

RCFB is a spouted bed with a central riser tube. The smaller central riser tube carries the particles upwards with the fluidizing gas and the outer tube carries the free falling particles downward. Though Circulating Fluidized Beds (CFBs) have been studied in detail, there are not many studies on RCFBs.

The present work is a study on the various aspects of a recirculating fluidized bed. A cold model semicircular recirculating fluidized bed was designed, fabricated and used for this study. Solid circulation rate, pressure drop across the various components of the reactor, gas bypassing and cluster formation and annular downflow layer are studied in detail for the various operating and design parameters.

The effects of particle size, spacing between the riser bottom and the air distributor, inventory of solids and air flow rate on the solid circulation rate were studied

experimentally. Increase in the inventory of bed materials and air flow rate generally lead to an increase in the solid circulation rate in a RCFB. There is an optimum spacing between the draft tube bottom and the distribution plate which gives the highest solid circulation rate. A mathematical model was developed for the solid circulation rate incorporating the effect of the various operating and design parameters. The model is based on the present experimental work and the data available in the literature for the same kind of RCFBs. Dimensional analysis and non-linear regression models were used to develop this model. The final model equation is a non-linear relationship between the solid circulation rate and different operating and design variables. The model gives good results for the same kind of systems and in the range in which the variables were verified.

The effect of various operating and design parameters on the pressure drop of a RCFB was also studied in detail. Pressure drop across the riser, across the downcomer and between the riser bottom and the downcomer bottom were measured. The different parameters considered were air flow rate, inventory of solids and spacing between the riser bottom and the distributor, and size of the sand particles (Geldart D and B). There was an increase in the pressure drop across the riser with an increase in the inventory of solids. The pressure drops across the riser and across the downcomer were high for the fine particles as compared to the coarse particles. There was an increase in the pressure drop with the increase in the spacing between the riser bottom and the distributor, possibly due to the increase in the gas bypassing. A mathematical model was developed for the pressure drop in the RCFB. The model for the pressure drop in the riser was developed on the basis of Bernoulli force balance equation. The major contribution in the

pressure drop across the riser was of the head. The acceleration and friction components increased with the increase in the superficial gas velocity.

Gas bypassing from the riser air supply towards the downcomer affects the flow behavior in a recirculating fluidized bed. Gas bypassing is calculated on the basis of the mathematical model and the effects of various parameters on gas bypassing were analyzed. There was a decrease in gas bypassing with an increase in the solids inventory for coarse as well as for fine particles. Gas bypassing increased with an increase in the spacing between the riser bottom and the distributor. There was a decrease in gas bypassing with a decrease in size of the particles.

Cluster formation in circulating fluidized beds is of prime importance as it significantly influences heat and mass transfer. The clusters near the wall of the riser form a continuous downflowing layer known as the annular layer. The present work describes the measurement of annular layer thickness in a recirculating fluidized bed using high speed video camera. The effect of various operational and design parameters on the annular downflow layer thickness was studied experimentally. Inventory of solids, air flow rate, particle size, axial height (measurement position in the riser) and the spacing between the distribution plate and riser bottom were the various operating and design parameters considered in this study. A frequency factor is defined which acts as an indicator of the stability of the annular downflow layer. A correlation between the annular layer thickness and the operating and design parameters was developed based on the experimental results. The correlation developed can be useful in the better understanding of the hydrodynamics of the RCFBs. The results indicate that annular layer thickness decreases with the increase in air flow rate as well as with the axial position

along the riser. The annular layer thickness increases with the increase in the spacing between the riser bottom and the distribution plate. Fine sand has relatively more stable annular downflow layer as compared to the coarse sand.

The present work can be useful for the optimization of the design and operation of recirculating fluidized bed reactors. The study can be used to design the various components of the reactor for desired solid circulation rate with more flexibility in choosing the different parameters. The pressure drop and gas bypassing study can be useful in the air/gas facility design. The annular downflow layer thickness model can be useful for the calculation of heat transfer and mixing coefficients.

CONTENTS

	Page No
Certificate	i
Acknowledgements	ii
Abstract	iv
Contents	viii
List of Figures	xiii
List of Tables	xviii
Nomenclature	xix
CHAPTER 1 INTRODUCTION	1-1
1.1 General	1-1
1.2 Fluidized Bed	1-1
1.2.1 Flow Regimes in Fluidized Beds	1-2
1.2.2 Applications of Fluidized Beds in Environmental Engineering	1-4
1.2.2.1 Fluidized Bed Incineration	1-4
1.2.2.2 Biological Treatment	1-7
1.2.2.3 Energy Recovery from Organic Wastes	1-9
1.2.2.4 Air Pollution Control	1-10
1.2.2.5 Fluidized Bed Combustion of Fuels for Power Generation	1-11
1.3 Circulating Fluidized Bed	1-13
1.4 Recirculating Fluidized Bed	1-13
1.5 Need for the Present Study	1-18
1.6 Objectives and Scope of the Study	1-19
1.6.1 Objectives	1-19
1.6.2 Scope	1-19
1.7 Overview of the Thesis	1-20
CHAPTER 2 RECIRCULATING FLUIDIZED BED-AN OVERVIEW	2-1
2.1 General	2-1

2.2	Design of Recirculating Fluidized Beds	2-1
2.2.1	Solid Circulation Rate	2-2
2.2.1.1	Measurement of Solid Circulation Rate	2-2
2.2.2	Distribution Plate	2-5
2.2.3	Downcomer – Riser Area Ratio	2-6
2.2.4	Riser – Air Jet Area Ratio	2-6
2.2.5	Spacing between Riser Bottom and Perforated Plate	2-7
2.2.6	Riser Height	2-7
2.2.7	Freeboard	2-8
2.3	Operations of Recirculating Fluidized Beds	2-8
2.3.1	Riser Voidage	2-9
2.3.2	Inventory of Solids	2-9
2.3.3	Air Velocity	2-10
2.3.4	Downcomer and Riser Pressure Drops	2-10
2.3.5	Gas Bypassing	2-11
2.3.5.1	Measurement of Gas Bypassing	2-12
2.3.6	Flow Regime in Riser of a RCFB	2-12
2.3.6.1	Clusters	2-13
2.3.6.2	Mechanism of Cluster Formation	2-14
2.3.6.3	Properties of Clusters	2-15
2.3.6.4	Measurement Techniques	2-17
2.3.6.5	Annular Downflow Layer	2-19
2.3.6.6	Mathematical Correlations for Annular Downflow Layer	2-20
2.4	Operational Difficulties and Troubleshooting	2-22
2.4.1	Start up Operation	2-22
2.4.2	Constriction at the Clearance	2-24
2.4.3	Mismatch of Solids flow from the Downcomer to the Riser and Particle Carrying Capacity of Jet	2-24
2.4.4	Operations under Sticky Conditions	2-25
2.5	Inferences from the Literature Review	2-26

CHAPTER 3	EXPERIMENTAL SETUP	3-1
3.1	Design and Fabrication of a Recirculating Fluidized Bed	3-1
3.2	Fluidizing Media and Fluidizing Gas	3-2
3.3	Measurement Methods for Various Parameters	3-5
3.4	Operation of RCFB Reactor	3-6
3.4.1	Minimum Solid Inventory Requirement	3-7
3.4.2	Superficial Gas Velocity Requirement	3-7
CHAPTER 4	SOLID CIRCULATION RATE IN A RCFB	4-1
4.1	General	4-1
4.2	Experimental Procedure	4-2
4.3	Results and Discussion	4-3
4.3.1	Effect of Air Flow Rate (Q_t)	4-3
4.3.2	Effect of Inventory (i)	4-7
4.3.3	Effect of Spacing between Riser Bottom and Gas Distributor (x)	4-10
4.3.4	Effect of Particle Size (d_p)	4-13
4.4	Mathematical Formulation	4-16
4.4.1	Construction of the Dimensionless Variables	4-17
4.4.2	Development of the Final Model Equation	4-19
4.4.3	Validation of the Model	4-21
4.4.4	Significance of the Model	4-23
4.5	Summary	4-26
CHAPTER 5	PRESSURE DROP IN A RCFB	5-1
5.1	General	5-1
5.2	Measurements and Computations	5-1
5.3	Experimental Results and Discussion	5-3
5.3.1	Effect of Inventory (i)	5-6
5.3.2	Effect of Particle Size (d_p)	5-10
5.3.3	Effect of Superficial Gas Velocity (U_0)	5-11
5.3.4	Effect of Spacing between Riser Bottom and Gas	5-15

	Distributor (x)	
5.4	Mathematical Model	5-15
5.4.1	Pressure Drop in the Riser	5-16
5.4.1.1	Model Formulation	5-16
5.4.1.2	Validation of Model	5-20
5.4.2	Pressure Drop across the Downcomer	5-23
5.5	Summary	5-24
CHAPTER 6	GAS BYPASSING IN A RCFB	6-1
6.1	General	6-1
6.2	Mathematical Evaluation	6-2
6.3	Effect of Various Parameters on Gas Bypassing	6-3
6.3.1	Effect of Air Flow Rate (Q_t)	6-3
6.3.2	Effect of Inventory of Solids (i)	6-7
6.3.3	Effect of Particle Size (d_p)	6-7
6.3.4	Effect of Spacing between Riser Bottom and Gas Distributor (x)	6-8
6.4	Summary	6-10
CHAPTER 7	ANNULAR DOWNFLOW LAYER IN A RCFB	7-1
7.1	General	7-1
7.2	Experimental Methodology	7-2
7.2.1	Measurement of Annular Downflow Layer	7-2
7.2.1.1	Video Capture	7-2
7.2.1.2	Video Frame Selection and Optimization	7-4
7.2.2	Frequency Factor	7-5
7.2.3	Selection of Operating and Design Parameters	7-5
7.3	Results and Discussion	7-7
7.3.1	Effect of Air Flow Rate (Q_t)	7-7
7.3.2	Effect of Axial Position (h)	7-11
7.3.3	Effect of Inventory (i)	7-12
7.3.4	Effect of Spacing between Riser Bottom and Distributor (x)	7-15

	Distribution Plate (x)	
7.3.5	Effect of Particle Size (d_p)	7-21
7.3.6	Effect of Solid Circulation Rate (W_s)	7-21
7.4	Mathematical Correlation	7-22
7.5	Summary	7-25
CHAPTER 8	CONCLUSIONS	8-1
8.1	Conclusions	8-1
8.2	Significance of Present Work	8-3
8.3	Limitations and Scope of Future work	8-4
REFERENCES		R-1
APPENDICES		
Appendix A:	Calculations of Terminal Velocity and Minimum Fluidization Velocity of Particles	A-1
Appendix B:	Experimental Results from the Literature and Present Study Used in the Development of the Model for Solid Circulation Rate	A-3
Appendix C:	Effect of Inventory on Pressure Drop in Riser of a RCFB	A-6
Appendix D:	Effect of Inventory on Pressure Drop in Downcomer in a RCFB	A-8
Appendix E:	Effect of Inventory on Pressure Drop between Riser Bottom and Downcomer Bottom of a RCFB	A-10
Appendix F:	Percentage Wise Pressure Drop in the Riser of a RCFB for Various Operating Conditions for Geldart D Particles	A-12
Appendix G:	Percentage Wise Pressure Drop in the Riser of a RCFB for Various Operating Conditions for Geldart B Particles	A-14
Appendix H:	% Gas Bypassing from Riser to Downcomer of a RCFB for Various Operating Conditions for Geldart D Particles	A-16
Appendix I:	% Gas Bypassing from Riser to Downcomer of a RCFB for Various Operating Conditions for Geldart B Particles	A-18
BIO-DATA		B-1