

**CATALYTIC VALORIZATION OF LIGNOCELLULOSIC
BIOMASS FOR THE PRODUCTION OF VALUABLE
CHEMICALS**

AKSHAY RAJU MANKAR



**DEPARTMENT OF CHEMICAL ENGINEERING
INDIAN INSTITUTE OF TECHNOLOGY DELHI
DECEMBER 2022**

© Indian Institute of Technology Delhi (IITD), New Delhi, 2022

**CATALYTIC VALORIZATION OF LIGNOCELLULOSIC
BIOMASS FOR THE PRODUCTION OF VALUABLE
CHEMICALS**

by

**AKSHAY RAJU MANKAR
DEPARTMENT OF CHEMICAL ENGINEERING**

Submitted

In fulfilment of the requirements of the degree of
DOCTOR OF PHILOSOPHY

to the



**INDIAN INSTITUTE OF TECHNOLOGY DELHI
DECEMBER 2022**

CERTIFICATE

This is to certify that the thesis entitled, “*Catalytic Valorization of Lignocellulosic Biomass for the Production of Valuable Chemicals*” being submitted by **Mr. Akshay Raju Mankar** in the fulfilment of requirements for the award of degree of **Doctor of Philosophy** to the Indian Institute of Technology Delhi, (India) is authentic record of work carried out by him. Mr. Akshay Raju Mankar has worked under my guidance and supervision and has fulfilled the requirements for the submission of this thesis, which to my knowledge has reached the requisite standard. The results contained in this thesis are original and have not been submitted, in part or full, to any other university or institute for the award of any other degree or diploma.



Prof. K. K. Pant

Professor,

Department of Chemical Engineering,

Indian Institute of Technology Delhi

ACKNOWLEDGEMENTS

I would like to express my heartiest gratitude, respect, and deep appreciation to **Prof. K. K. Pant** (Professor, Department of Chemical Engineering, IIT Delhi) under whose able guidance I ventured to undertake this effort. I am grateful to him for his valuable guidance, indispensable suggestions, constant encouragement, constructive criticism, and moral support, without which it had not been possible for me to reach this level of achievement in the work.

I am extremely thankful to **Prof. A. K. Saroha**, Head of Department, for providing necessary facilities and support to carry out the work. I would like to extend my sincere gratitude to members of SRC especially **Prof. A. K. Saroha, Prof. Divesh Bhatia, Prof. S. N. Naik** for their valuable suggestions and critical review of my work. I gratefully acknowledge the central research facility (CRF) and IIT Delhi for providing me an excellent academic environment and facilities to carry out this work effectively.

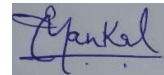
I take this opportunity to specially thank my fellow lab members and seniors **Dr. Ashish, Dr. Arindam, Dr. Ejaz, Dr. Shireen, Mr. Rohit, Mr. Sonit, Mr. Sourabh, Mr. Kaushal, Mr. Prashant, Ms. Uma, Mr. Rajan, Ms. Komal, Mr. Ramdayal, Mr. Sagar, Ms. Vallari, and all my juniors** from Catalytic Reaction Engineering laboratory for their enthusiastic support, time to time help, and encouragement during my research work. I would especially like to thank my dear friends **Ms. Deepti and Mr. Marut** for always being there for me and providing joyous environment during the entire period of my research work. I would like to extend my thanks to lab staff **Mr. Vishesh, Mr. Suchit, Mr. Krishan, Mr. Vijaypal, Mr. Ashish and other staff members** of the Department of Chemical Engineering for their help and support during the entire period of my work.

The financial assistance from Science and Engineering Research Board (SERB), Department of Science and Technology (DST), and IIT Delhi is gratefully acknowledged, without which the present research work would not have been completed.

It is my pleasure to express my heartiest appreciation to my beloved family members. My abilities and positive attitude towards life are all because of my family. I bow sacred reverence to my parents **Dr. Raju B. Mankar** and **Mrs. Utpala R. Mankar** who have always been my idol and I am blessed to have them in my life. I am thankful to them for always supporting me, teaching me to stay positive, and showing me the right path during my difficult times. Their blessings and love always provided me strength and enthusiasm to do something more with perfection. I would like to thank my brother **Mr. Nilay R. Mankar** and sister-in-law **Mrs. Dhanashree N. Mankar** for being by my side during my good and bad times throughout my life and career. I would like to thank my fiancé **Ms. Vaishnavi Pathak** for supporting me and always being there for me at all times. At this juncture today, I dedicate this thesis to my beloved family members.

I humbly bow before GOD almighty for showering the blessings and giving me patience, peace, strength, perseverance, throughout the journey of my life.

I pay my sincere thanks to all those who were directly or indirectly involved in the completion of this work.



AKSHAY RAJU MANKAR

ABSTRACT

The rising fuel prices along with the numerous climatic concerns such as global warming, acid rains, melting of glaciers, etc, severely affect the incessant use of fossil reserves. By the year 2040, it is expected that the exponential rise in energy demands will be enhanced significantly by about 28% of its present value. Lignocellulosic biomass (LCB) is an attractive alternative due to its abundancy and its ability to produce a wide range of fuels and chemicals. Considering the availability of LCB in India (~ 750 million tons), LCB conversion to fuels and feedstocks is significant to tackle the burning clean energy issues. LCB consists of complex networks containing cellulose (30-50%), hemicellulose (20-35%), and lignin (15-30%). A wide range of chemicals e.g., sorbitol, xylitol, ethylene glycol, 5-hydroxymethylfurfural, levulinic acid, guaiacol, vanillin, phenols, etc, can be extracted *via* different reactions viz., dehydration, hydrogenation, oxidation, hydrolysis, hydrodeoxygenation, retro-aldol condensation, etc, in the presence of catalysts.

This thesis is focussed on development of efficient catalysts for valorization of all the three components of LCB which will be beneficial for the commercialization of sustainable future bio-based refineries. Investigation of one-pot hydrolytic hydrogenation of cellulose to ethylene glycol and hexitols by a combination of heteropolyacid/ZrO₂ and Ru/C was done. The heterogeneous system produces 26.5% hexitol and 40% ethylene glycol yield. Mechanistically, it was also proved that initial hydrolysis of cellulose to glucose followed by the formation of glycolaldehyde was also accomplished by heteropolyacid/ZrO₂ support. The intermediate glycolaldehyde and glucose was successively reduced to ethylene glycol and hexitols, respectively, by Ru/C. Moreover, prior treatment of cellulose by ball-milling reduces its crystallinity and thus accounts to high conversion to cellulose. In another study, organic-

inorganic hybrid metal-free sulfonated porphyrin-based porous organic polymer was synthesized for the production of 5-hydroxymethylfurfural (HMF) from fructose in water. The research is advantageous and shows high HMF yield of 85% in water, therefore bypassing the use of toxic organic solvents. Incorporation of silica introduces hydrophilicity as well as inter-particle mesopores to enhance interaction and diffusion of bulky substrates like fructose, resulting in high HMF yield. Acid/base bifunctional organocatalyst was developed for direct conversion of glucose to HMF in water giving a HMF yield of 60% under optimum conditions. A thorough kinetic modelling was also done and the values predicted by the developed model were found to give an excellent fit with the experimental data. Environmentally-friendly deep eutectic solvents (DESs) were also synthesized and applied for the synthesis of HMF. HMF yield of 88% was achieved when the reaction was performed under the microwave irradiation at 140 °C for 30 min in the presence of acetone: water and choline chloride (ChCl): lactic acid (LA) DES. The release of H⁺ from the DES was favored due to competing hydrogen bonding interactions between OH group of lactic acid and fructose, which promoted the dehydration of fructose to HMF. Furthermore, DESs have also been utilized for the pretreatment of LCB to extract lignin in high purity without much alteration in its native structure. Under optimum conditions (150 °C, 20 min, ChCl: LA DES), lignin yield of 82% was achieved using microwave heating. A study was also done to show the advantages of Ru-single atoms for one-pot hydrogenation of xylose and glucose to xylitol and sorbitol, respectively. The use of Ru-single atom shows significant advantages over Ru-NPs supported catalysts for the hydrogenation of sugar molecules using hydrogen donor solvents and thus avoiding the use of high-pressure external hydrogen. Under such context, Ru-single atom catalyst enables steady production of xylitol with 95% yield. This research deals a mild protocol to utilize biomass-feedstocks for producing commercially important low-calorie sugars.

सारांश

वैश्विक तापमान वृद्धि, अम्ल वर्षा, ग्लेशियरों के पिघलने आदि जैसी कई जलवायु संबंधी चिंताओं के साथ बढ़ती ईंधन की कीमतें जीवाश्म भंडार के निरंतर उपयोग को गंभीर रूप से प्रभावित करती हैं। वर्ष 2040 तक, यह उम्मीद की जाती है कि ऊर्जा मांगों में घातीय वृद्धि इसके वर्तमान मूल्य के लगभग 28% तक बढ़ जाएगी। लिग्नोसेल्यूलोसिक बायोमास (एलसीबी) इसकी प्रचुरता और ईंधन और रसायनों की एक विस्तृत श्रृंखला का उत्पादन करने की क्षमता के कारण एक आकर्षक विकल्प है। भारत में एलसीबी की उपलब्धता (~ 750 मिलियन टन) को ध्यान में रखते हुए, जलती हुई स्वच्छ ऊर्जा के मुद्दों से निपटने के लिए ईंधन और फीडस्टॉक्स में एलसीबी रूपांतरण महत्वपूर्ण है। एलसीबी में जटिल नेटवर्क होते हैं जिनमें सेल्युलोज (30-50%), हेमिकेलुलोज (20-35%), और लिग्निन (15-30%) होते हैं। रसायनों की एक विस्तृत श्रृंखला जैसे, सोर्बिटोल, ज़ाइलिटोल, एथिलीन ग्लाइकॉल, 5-हाइड्रॉक्सीमिथाइलफ्यूरफ्यूरल, लेवुलिनिन एसिड, गुआयाकोल, वैनिलिन, फिनोल, आदि को विभिन्न प्रतिक्रियाओं जैसे निर्जलीकरण, हाइड्रोजनीकरण, ऑक्सीकरण, हाइड्रोलिसिस, हाइड्रोडीऑक्सीजनेशन, उत्प्रेरकों की उपस्थिति में एल्डोल संघनन आदि माध्यम से निकाला जा सकता है।

यह शोध कार्य एलसीबी के सभी तीन घटकों के मूल्यांकन के लिए कुशल उत्प्रेरक के विकास पर केंद्रित है जो भविष्य की जैव-आधारित रिफाइनरियों के व्यावसायीकरण के लिए फायदेमंद होगा। हेटेरोपॉलीएसिड/ ZrO_2 और Ru/C के संयोजन द्वारा एथिलीन ग्लाइकॉल और हेक्सिटोल में सेल्युलोज

के एकक हाइड्रोलाइटिक हाइड्रोजनीकरण की जांच की गई। विषम प्रणाली 26.5% हेक्सिटोल और 40% एथिलीन ग्लाइकॉल का उत्पादन करती है। यंत्रवत् रूप से, यह भी साबित हो गया था कि ग्लाइकोलाडिहाइड के गठन के बाद सेल्युलोज के ग्लूकोज के प्रारंभिक हाइड्रोलिसिस को भी हेटरोपॉलीएसिड / ZrO₂ समर्थन द्वारा पूरा किया गया था। मध्यवर्ती ग्लाइकोलडिहाइड और ग्लूकोज क्रमशः Ru/C द्वारा एथिलीन ग्लाइकॉल और हेक्सिटोल में क्रमशः कम हो गए थे। इसके अलावा, बॉल-मिलिंग द्वारा सेल्युलोज के पूर्व उपचार से इसकी क्रिस्टलीयता कम हो जाती है और इस प्रकार सेल्युलोज में उच्च रूपांतरण होता है। एक अन्य अध्ययन में, पानी में फ्रुक्टोज से 5-हाइड्रॉक्सीमिथाइलफुरफुरल (HMF) के उत्पादन के लिए कार्बनिक-अकार्बनिक संकर धातु-मुक्त सल्फोनेटेड पोर्फिरिन-आधारित कार्बनिक बहुलक को संश्लेषित किया गया था। अनुसंधान फायदेमंद है और पानी में 85% की उच्च एचएमएफ उपज दिखाता है, इसलिए जहरीले कार्बनिक विलायक के उपयोग को दरकिनार कर देता है। सिलिका को शामिल करने से हाइड्रोफिलिसिटी के साथ-साथ अंतर-कण सतह छिद्रों का परिचय होता है, जिससे फ्रुक्टोज जैसे भारी सबस्ट्रेट्स के संपर्क और प्रसार में वृद्धि होती है, जिसके परिणामस्वरूप उच्च एचएमएफ की प्राप्ति होती है।

अम्ल/क्षार बाइफंक्शनल ऑर्गेनोकैटेलिस्ट को पानी में ग्लूकोज के एचएमएफ में सीधे रूपांतरण के लिए विकसित किया गया था, जिससे इष्टतम परिस्थितियों में 60% एचएमएफ उपज मिलती है। एक संपूर्ण काइनेटिक मॉडलिंग भी किया गया था और विकसित मॉडल, अनुमानित मूल्य प्रयोगात्मक डेटा के साथ एक उत्कृष्ट फिट देने के लिए पाए गए थे। एचएमएफ के संश्लेषण के लिए पर्यावरण के अनुकूल गहरे

ईयूटेक्टिक सॉल्वेंट्स (डीईएस) को भी संश्लेषित किया गया था। एसीटोन: पानी और कोलीन क्लोराइड (ChCl): लैक्टिक एसिड (LA) DES की उपस्थिति में 30 मिनट के लिए 140 ° C पर माइक्रोवेव विकिरण के तहत प्रतिक्रिया करने पर 88% की HMF उपज प्राप्त हुई। डीईएस से एच + की रिहाई को लैक्टिक एसिड और फ्रुक्टोज के ओएच समूह के बीच प्रतिस्पर्धात्मक हाइड्रोजन बॉन्डिंग इंटरैक्शन के कारण पसंद किया गया, जिसने एचएमएफ को फ्रुक्टोज के निर्जलीकरण को बढ़ावा दिया। इसके अलावा, डीईएस का उपयोग एलसीबी के प्रीट्रीटमेंट के लिए भी किया गया है ताकि उच्च शुद्धता में लिग्निन निकालने के लिए इसकी मूल संरचना में बहुत बदलाव किए बिना। इष्टतम स्थितियों (150 डिग्री सेल्सियस, 20 मिनट, ChCl: LA DES) के तहत, माइक्रोवेव हीटिंग का उपयोग करके 82% की लिग्निन उपज प्राप्त की गई। ज़ाइलोज के एक-पॉट हाइड्रोजनीकरण और ज़ाइलिटोल और सोर्बिटोल के ग्लूकोज के क्रमशः आरयू-एकल परमाणुओं के लाभों को दिखाने के लिए एक अध्ययन भी किया गया था। हाइड्रोजन डोनर सॉल्वेंट्स का उपयोग करके चीनी अणुओं के हाइड्रोजनीकरण के लिए आरयू-एनपी समर्थित उत्प्रेरकों पर आरयू-सिंगल परमाणु का उपयोग महत्वपूर्ण लाभ दिखाता है और इस प्रकार उच्च दबाव वाले बाहरी हाइड्रोजन के उपयोग से बचा जाता है। ऐसे संदर्भ में, आरयू-एकल परमाणु उत्प्रेरक 95% उपज के साथ xylitol के स्थिर उत्पादन को सक्षम बनाता है। यह शोध व्यावसायिक रूप से महत्वपूर्ण कम कैलोरी शर्करा के उत्पादन के लिए बायोमास-फीडस्टॉक्स का उपयोग करने के लिए एक हल्के प्रोटोकॉल से संबंधित है।

TABLE OF CONTENT

TITLE	PAGE
Certificate	I
Acknowledgements	II
Abstract	IV
Table of Content	VI
List of Figures	XII
List of Tables	XVII
List of Abbreviations	XIX
1 Introduction	1-9
1.1 Background and motivation	1
1.2 Composition of Lignocellulosic biomass and its valorization to valuable chemicals	3
1.2.1 Cellulose	4
1.2.2 Hemicellulose	6
1.2.3 Lignin	7
1.3 Thesis organization	8
2 Literature review	10-94
2.1 Background	10
2.2 Synthesis of HMF	11
2.2.1 Homogeneous catalysts	12
2.2.2 Heterogeneous catalysts	17
2.3 Synthesis of sorbitol, xylitol, ethylene glycol	22
2.4 Valorization of lignin	31
2.4.1 Thermal depolymerization of lignin	33
2.4.1.1 Pyrolysis of lignin	34
2.4.1.2 Gasification of lignin	37
2.4.2 Thermo-catalytic depolymerization of lignin	38
2.4.2.1 Oxidative depolymerization of lignin	38
2.4.2.2 Reductive depolymerization of lignin	47
2.5 The concept of “Lignin first” process for lignin	51

valorization	
2.6	Economic analysis of lignin valorization 61
2.7	Pretreatment of Lignocellulosic biomass 63
2.7.1	Physical pretreatment methods 64
2.7.1.1	Milling pretreatment 65
2.7.1.2	Extrusion pretreatment 66
2.7.1.3	Microwave pretreatment 67
2.7.1.4	Ultrasound pretreatment 70
2.7.2	Chemical pretreatment methods 72
2.7.2.1	Acid pretreatment 72
2.7.2.2	Alkali pretreatment 73
2.7.2.3	Organosolv pretreatment 75
2.7.2.4	Co-solvent enhanced lignocellulosic fractionation 76
2.7.2.5	Ammonia fiber explosion 78
2.7.2.6	Ionic liquids 80
2.7.2.7	Deep eutectic solvents 84
2.8	Gaps in literature 91
2.9	Hypothesis 92
2.10	Objectives 94
2.10.1	Overall objective 94
2.10.2	Specific objectives 94
3	Experimental details and methodology 95-115
3.1	Background 95
3.2	Materials 95
3.3	Methods 97
3.3.1	Catalyst synthesis procedures 97
3.3.1.1	Synthesis of heteropolyacid/ZrO ₂ 97
3.3.1.2	Synthesis of deep eutectic solvents 97
3.3.1.3	Synthesis of sulfonated porphyrin-based porous organic polymer 98
3.3.1.4	Synthesis of acid-based grafted caged silica 99
3.3.1.5	Synthesis of phosphine containing porous ligand 100
3.3.1.6	Synthesis of Ru-PPh 100
3.3.1.7	Synthesis of ruthenium-catechol-based porous ligand 101

3.3.1.8	Synthesis of ruthenium-based triphenylamine containing porous ligand	101
3.3.1.9	Synthesis of silica templates	101
3.3.1.10	Synthesis of silica/polymer composite	102
3.3.1.11	Synthesis of template-free ordered polymers	102
3.3.1.12	Synthesis of Ru-loaded ordered polymers	103
3.3.2	Catalyst characterization	103
3.3.3	Characterization of microcrystalline cellulose	105
3.4	Experimental procedures	107
3.4.1	Hydrolytic hydrogenation of MCC and hydrogenation of glucose using HPA/ZrO ₂	107
3.4.2	One-Pot Conversion of Fructose to HMF using PorPOPS catalyst	108
3.4.3	One-Pot Conversion of Fructose to HMF using DES	109
3.4.4	One-Pot Conversion of Glucose to HMF using Si-AB catalyst	110
3.4.5	Xylose /Glucose hydrogenation using Ru-PPh-MesoSi	111
3.4.6	Extraction of lignin from coconut coir using DES	111
3.4.7	Depolymerization of extracted lignin by catalytic transfer hydrogenation	112
3.4.8	Product analysis	113
4	Synthesis of sorbitol, xylitol, ethylene glycol from biomass-based feedstocks	116-156
4.1	Overview: One-pot conversion of cellulose to hexitols and ethylene glycol using heteropolyacid/zirconia	116
4.2	Background and introduction	117
4.3	Results and discussion	118
4.3.1	Characterization of untreated and ball-mill treated microcrystalline cellulose	118
4.3.2	Characterization of catalysts	121
4.3.3	Catalytic conversion of cellulose to hexitols and ethylene glycol	126
4.3.3.1	Effect of ball-milling	126
4.3.3.2	Role of catalyst in product distribution	128

4.3.3.3	Effect of reaction temperature and catalyst recyclability	130
4.3.3.4	Reaction pathway for microcrystalline cellulose conversion	134
4.4	Conclusions	135
4.5	Overview: Synthesis of artificial sweeteners using Ru-single atom on mesoporous phosphine polymer catalyst	156
4.6	Background and introduction	137
4.7	Results and discussion	139
4.7.1	Synthesis and characterizations	139
4.7.2	Catalytic activity test	150
4.8	Conclusion	155
5	Catalytic conversion of fructose/glucose to 5-hydroxymethylfurfural	157-210
5.1	Overview: Conversion of fructose to 5-hydroxymethylfurfural using sulfonated mesoporous porphyrin catalyst in water	157
5.2	Background and introduction	158
5.3	Results and discussion	160
5.3.1	Catalyst characterization	160
5.3.2	Performance of the catalysts	165
5.4	Conclusions	169
5.5	Overview: Conversion of fructose to 5-hydroxymethylfurfural using deep eutectic solvents as catalyst	170
5.6	Background and introduction	170
5.7	Results and discussion	174
5.7.1	Characterization of deep eutectic solvents	174
5.7.2	Experimental results	176
5.7.2.1	Initial screening of deep eutectic solvents	176
5.7.2.2	Effect of reaction time	178
5.7.2.3	Effect of solvent	179
5.7.2.4	Effect of reaction temperature	180
5.7.2.5	Effect of fructose concentration and deep eutectic solvent dosage	181

5.7.2.6	Recycling of deep eutectic solvent	182
5.7.2.7	Comparison of heating methods	183
5.7.2.8	Significance of hydrogen bond acceptor and hydrogen bond donor in deep eutectic solvents for fructose dehydration	185
5.8	Conclusion	187
5.9	Overview: Conversion of glucose to 5-hydroxymethylfurfural using acid/base bi-functional silica nanocage as catalyst in water and its kinetic modelling	188
5.10	Background and introduction	189
5.11	Results and discussion	192
5.11.1	Catalyst synthesis and characterizations	192
5.11.2	Experimental results	199
5.11.3	Kinetic model	203
5.11.4	Kinetic study	204
5.12	Conclusions	209
6	Pretreatment of biomass and lignin valorization to aromatics	211-232
6.1	Overview: Pretreatment of biomass using deep eutectic solvents for lignin extraction and its valorization to aromatics	211
6.2	Background and introduction	211
6.3	Results and discussion	215
6.3.1	Pretreatment of coconut coir for lignin extraction	215
6.3.1.1	Screening of DESs for lignin extraction	215
6.3.1.2	Effect of reaction temperature and time on lignin extraction	218
6.3.1.3	Effect of molar ratio of choline chloride to lactic acid on lignin extraction	221
6.3.1.4	Comparison of conventional and microwave heating and deep eutectic solvent recyclability	222
6.3.2	Characterization of extracted lignin and raw coconut coir	224
6.3.3	Optimization of reaction parameters for catalytic transfer	229

	hydrogenation	
6.4	Conclusions	232
7	Conclusions and future recommendations	233-237
7.1	Conclusions	233
7.2	Future recommendations	236
	References	238
	Appendices	278
	Actual images of the reactors	278
	Publications	281
	Biodata	284

LIST OF FIGURES

FIGURE NO.	FIGURE CAPTION	PAGE NO.
1.1	Global primary energy consumption	2
1.2	Typical composition of Lignocellulosic biomass	4
1.3	Structural representation of cellulose	5
1.4	Overview of valorization of lignocellulosic biomass for the production of valuable chemicals and their applications	5
1.5	Monomers of hemicellulose	6
1.6	Plausible structure of lignin and monolignols present in lignin	7
2.1	A reaction pathway for the conversion of cellulose to 5-hydroxymethylfurfural	12
2.2	A reaction pathway for the synthesis of sorbitol, xylitol, ethylene glycol	23
2.3	(a) A representative structure of lignin with common inter-unit linkage and plausible valorization products, (b) Overview of lignin valorization for future biorefineries	32
2.4	Overview of lignin depolymerization methods	33
2.5	(a) Major products obtained from oxidative depolymerisation of lignin, (b) Reaction pathway for vanillin conversion to 2-methoxy phenol, (c) Reaction pathway for HDO of guaiacol	48
2.6	Different types of pretreatment methods for the LCB fractionation	64
4.1	(a) XRD patterns of MCC ball-milled at different conditions, (b) ATR-FTIR spectra of MCC ball-milled at different conditions	119
4.2	(a) ATR-FTIR spectra of raw and ball-milled MCC, FESEM of (b) raw MCC, (c) ball-milled (900 rpm, 8 h) MCC	121
4.3	(a) XRD patterns, (b) NH ₃ -TPD profiles	122
4.4	(a,b,c) Parent HPA and HPA supported on ZrO ₂ , ATR-FTIR spectra, (d,e,f) Raman spectra	124
4.5	Raman spectra of ZrO ₂ support	125

4.6	FESEM-EDX with elemental mapping (a) ZrO ₂ , (b) PTA/ZrO ₂ , (c) STA/ZrO ₂ , (d) PMA/ZrO ₂	126
4.7	Influence of ball-milling pretreatment of MCC on the conversion and product yield	127
4.8	(a) Effect of temperature on the product yield, (b) Effect of catalyst recyclability on the product yield	131
4.9	Most possible reaction pathway for the conversion of cellulose using PTA/ZrO ₂ and Ru/C catalysts to produce hexitols and ethylene glycol	135
4.10	Schematic representation for the synthesis and most possible structures of Ru single-atoms based porous organic ligands	140
4.11	TGA spectra of template-free silica precursors and the corresponding Ru-catalysts, performed under air atmosphere	141
4.12	Low angle X-ray diffraction patterns of (a) MesoSi (red), CTAB template extracted MesoSi (black); (b) HF-treated Ru-PPh-MesoSi (blue); (c,d) comparative N ₂ sorption isotherm and (e,f) pore size distribution of different catalysts	142
4.13	(a) XRD of SBA-15 in black and SBA-15 templated Ru-PPh-SBA in red; (b) Wide-angle X-ray diffraction (WAXS) of template free MesoSi (black); Ru-PPh (blue) and Ru-PPh-MesoSi (red)	143
4.14	HRTEM and FESEM of catalyst	144
4.15	(a) N ₂ sorption adsorption (closed) and desorption (open) isotherm of microporous Ru-catalysts synthesized without using silica templates; (b) Pore size distribution; black (Ru-Cat); blue (Ru-PPh); red (Ru-AmPh)	145
4.16	FT-IR spectra of (a) template-free MesoSi, Ru-Cat, and (b) Ru-PPh and Ru-AmPh	147
4.17	(a) Deconvoluted Ru 3 <i>p</i> core-level spectra (i) Ru-AmPh, (ii) Ru-Cat, (iii) Ru-PPh-MesoSi; deconvoluted (b) C1s and (c) O1s; (d) P 2 <i>p</i> of Ru-PPh-MesoSi	148
4.18	(a) ³¹ P CP-MAS NMR; (b) <i>in-situ</i> CO-adsorption DRIFTS; (c) CO-adsorption DRIFTS of (1) Ru-PPh and (2) Ru-AmPh	149
4.19	HAADF-STEM image of (a) Ru-PPh-MesoSi, (b) pristine Ru-PPh	150

4.20	(a) Schematic representation for xylose hydrogenation routes; (b) Effect of TA (Triethylamine)/FA (Formic acid) ratio on xylitol yield; (c) showing xylitol yield and (d) conversion of xylose and selectivity of xylitol	151
4.21	Temperature effect on the hydrogenation of (a) xylose and (b) glucose	154
4.22	(a) Schematic presentation for glucose hydrogenation pathway, (b) Comparative study for one-pot glucose hydrogenation to sorbitol; (c) Conversion of glucose and the selectivity to sorbitol; (d) reusability study of xylose and glucose hydrogenation reactions	155
5.1	Schematic representation for the synthesis of PorPOPS	160
5.2	(a-b) N ₂ -sorption isotherm; (c-d) Pore size distribution; (e) FTIR-spectra and (f) TGA (air) analysis	161
5.3	(a) TEM and (b) FESEM image of FePOP-1; (c,d) TEM image of PorPOPS	162
5.4	(a,b) FESEM images of PorPOPS, (c) FePOP-1S, (d) un-functionalized PorPOP	163
5.5	XPS spectra of (a) N1s of PorPOP, (b,c,d) PorPOPS containing N1s, O1s and S2p	164
5.6	One-pot green conversion of fructose to HMF using PorPOPS	165
5.7	(a) Effect of temperature, (b) time and (c) catalyst dosage	166
5.8	Recyclability study of (a) PorPOPS and (b) FePOP-1S for fructose dehydration reaction to HMF	167
5.9	(a) Structures of the components used in DESs synthesis, (b) reaction pathway for dehydration of fructose to 5-HMF and side-products	173
5.10	FTIR spectra of (a) ChCl:Lactic acid DES, (b) ChCl:Acetic acid DES	174
5.11	FTIR spectra of (a) ChCl:Butyric acid DES, (b) ChCl:Glutaric acid DES	175
5.12	FTIR spectra of (a) ChCl:Urea DES, (b) freshly synthesized ChCl:LA DES and recycled ChCl:LA DES after fifth cycle	176
5.13	(a) Initial screening of DES-based on the 5-HMF yield, (b) Effect of reaction time on 5-HMF yield	178
5.14	(a) Effect of solvent on 5-HMF yield, (b) Effect of reaction temperature on 5-HMF yield	179

5.15	Effect of ChCl:LA DES recycling on 5-HMF yield	183
5.16	(a) Effect of heating method on 5-HMF yield, (b) Effect of ChCl, LA, B:LA, ChCl:LA as catalyst on 5-HMF yield	185
5.17	Synthesis protocol for acid/base bifunctional silica nanocage (Si-AB)	192
5.18	HR-TEM images of (a,b) caged silica, SiC; (c) Si-AB	193
5.19	FESEM and EDX of (a,d) caged silica; (b,e) NH ₂ -SiC; (c,f) Si-AB	194
5.20	N ₂ -adsorption (closed)/desorption (open) isotherm and the corresponding NLDFT pore size distribution of (a,c) SiC and (b,d) Si-AB	195
5.21	(a) FT-IR spectra of SiC, NH ₂ -SiC and Si-AB; (b) ¹³ C CP and (c) ²⁹ Si MAS NMR spectra of bifunctional Si-AB	196
5.22	(a) XPS survey spectrum, (b) C1s, (c) N1s; (d) CO ₂ -TPD and (e) NH ₃ -TPD of Si-AB catalyst	197
5.23	Representation for the plausible pathway for glucose dehydration to HMF and other by-products	200
5.24	Effect of reaction temperature (a) 150 °C, (b) 160 °C, (c) 170 °C on conversion of glucose, yield of fructose, yield of HMF at 0.5 h to 4 h	201
5.25	(a) Effect of catalyst dosage on the conversion of glucose, yield of fructose, yield of HMF, (b) Effect of different biomass-based carbohydrate substrates on yield of HMF	202
5.26	Reaction pathway for glucose conversion to HMF	203
5.27	Arrhenius plot for determination of activation energy and pre-exponential factor for three different reaction temperatures 150 °C, 160 °C, and 170 °C at (a) rate constant k ₁ , (b) rate constant k ₂	207
5.28	Fit between experimental data (symbols) and model predicted data (line) for variation in concentration (mol/L) of glucose, fructose, and HMF with reaction time at (a) 150 °C, (b) 160 °C, (c) 170 °C	208
5.29	Parity plot for experimental and model predicted data of concentration (mol L ⁻¹) of glucose, fructose, and HMF at 150 °C, 160 °C, 170 °C	209
6.1	(a) Screening of ChCl-based DESs with different HBDs, (b) Effect of temperature, (c) Effect of time, (d) Effect of ChCl: LA molar ratio on the lignin extraction from coconut coir using	217

	ChCl: LA DES	
6.2	FTIR spectra of (a) Kraft lignin and lignin extracted using ChCl: LA DES, (b) raw coconut coir and coconut coir recovered after the ChCl: LA DES pretreatment, (c) TGA profiles of Kraft lignin and lignin extracted using ChCl: LA DES, (d) DTG profile of Kraft lignin and lignin extracted using ChCl: LA DES	226
6.3	FESEM images at different magnifications of (a, b, c) Untreated raw coconut coir and (d, e, f) Coconut coir recovered after pretreatment with ChCl: LA DES	228

LIST OF TABLES

TABLE NO.	TABLE CAPTION	PAGE NO.
1.1	Typical composition of Lignocellulosic biomass from different sources	3
2.1	Homogeneous catalysts for the synthesis of 5-HMF from different bio-based substrates	16
2.2	Heterogeneous catalysts for the synthesis of 5-HMF from different bio-based substrates	19
2.3	Catalysts used for the synthesis of sorbitol, xylitol, ethylene glycol from different bio-based substrates	27
2.4	Microwave pyrolysis of different feedstocks and the bio-oil yield	36
2.5	Oxidative depolymerization of lignin/lignin model compounds using different catalysts	41
2.6	Reductive depolymerization of lignin/lignin model compounds using different catalysts	53
2.7	Solubility of lignin in ILs	81
2.8	Delignification of different biomass feedstocks using ILs	85
2.9	Delignification of different biomass feedstocks using DESs	88
3.1	DESs with molar ratios of ChCl (HBA) and HBDs	98
4.1	Effect of ball-milling pretreatment on the crystallite size and CrI of MCC	118
4.2	Acidity of the synthesized catalysts	123
4.3	Effect of different catalysts on the product yield	129
4.4	Comparative study among different catalysts for one pot hydrolytic hydrogenation of cellulose	132
5.1	Comparative study for PorPOPS in fructose conversion to HMF in water	168
5.2	Screening of DESs for dehydration of fructose to 5-HMF	177

5.3	Effect of fructose concentration and ChCl:LA DES dosage on 5-HMF yield Effect of reaction temperature on 5-HMF yield	182
5.4	Comparison of our results with the recent studies reported for dehydration of fructose to 5-HMF using different catalysts	186
5.5	Reaction rate constants based on the proposed model for HMF synthesis	205
5.6	Activation energy and pre-exponential factors for HMF synthesis	206
6.1	DESs with molar ratios of ChCl (HBA) and HBDs	215
6.2	Kamlet Taft solvatochromic parameters (α , β , and π^*) for the synthesized DESs	216
6.3	H factor for the pretreatment of coconut coir using DES under different reaction conditions	220
6.4	Effect of reaction parameters on CTH of lignin extracted using ChCl: LA DES from coconut coir	230

LIST OF ABBREVIATIONS

1,2-dichloroethane	DCE
1-alkyl-3-methylimidazolium chloride	[EMIM]Cl
1-butyl-3-methylimidazolium hexafluorophosphate	[BMIM]PF ₆
1-butyl-3-methyl-imidazolium tetrafluoroborate	[BMIM ⁺ BF ₄ ⁻]
2,5- dimethylfuran	DMF
2,5-bis(hydroxymethyl)furan	BHMF
2,5-diformylfuran	DFF
2,5-dimethyltetrahydrofuran	DMTF
2,5-furandicarboxylic acid	FDCA
3-(aminopropyl) triethoxysilane	APTES
4-nitroaniline	NA
5-hydroxymethylfurfural	5-HMF
acid/base bifunctional organocatalyst	Si-AB
activation energy	E _a
ammonia fiber explosion	AFEX
bond dissociation energy	BDE
carbon black	CB
carbon nanotubes	CNTs
catalytic transfer hydrogenation	CTH
catechol	Cat
cellulase secreting bacterial pretreatment	CBP
choline chloride	ChCl
co-solvent enhanced lignocellulosic fractionation	CELF
Deep eutectic solvents	DESs
difuctose anhydride	DFA
dimethoxymethane	DMM
Dimethyl sulfoxide	DMSO

dry ball milling method	DBM
Heteropolyacids	HPAs
hydrodeoxygenation	HDO
hydrogen bond acceptor	HBA
hydrogen bond donor	HBD
hydrothermal upgrading	HyThUp
Ionic liquids	ILs
lactic acid	LA
levoglucosan	LGA
lignin carbohydrate complex	LCC
lignocellulosic biomass	LCB
liquid ammonia pretreatment	LAT
liquid-to-solid ratio	LSR
metal-organic frameworks	MOFs
methyl ethyl ketone	MEK
microcrystalline cellulose	MCC
Microwave	MW
minimum ethanol selling price	MESP
Mobil composition of matter	MCM
N, N-diethyl-4- nitroaniline	DENA
nanoparticles	NPs
oil palm empty fruit bunch	OPEFB
para-toluene sulfonic acid	PTSA
p-coumaric acid	PCA
phosphomolybdic acid	PMA
phosphotungstic acid	PTA
polycyclic aromatic hydrocarbons	PAHs
polyoxometallates	POM
sulfonated porphyrin-based porous organic polymer	PorPOPS
prairie cord grass	PCG

pre-exponential factor	A
ruthenium-based triphenylamine containing porous ligand	Ru-AmPh
ruthenium-catechol-based porous ligand	Ru-Cat
silicoalumoniphosphate	SAPO
silicotungstic acid	STA
soyabean hulls	SH
spent coffee waste	SCW
sugarcane bagasse	SB
tetraethylammonium chloride	TEAC
Tetraethylorthosilicate	TEOS
Tetrahydrofuran	THF
triphenylamine	A
triphenylphosphine	PPh
wet disk milling	WDM